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Evaluation of Grewa Venusta (Wild Jute Tree) Extract as Corrosion Inhibitor for Mild Steel in Acidic Environment

I.Y. Suleiman,^{a,*} Sani A. Salihu,^b O.S. Emokpaire,^a

O.C. Ogheneme^c and Lasisi Shuaibu^a

 ^a Department of Metallurgical Engineering, Waziri Umaru Federal Polytechnic, Birnin Kebbi, Kebbi State, Nigeria
 ^b Department of Mechanical Engineering, Faculty of Engineering, Kebbi State University of Science and Technology, Aliero, Kebbi State, Nigeria
 ^c Department of Mechanical Engineering, Waziri Umaru Federal Polytechnic, Birnin Kebbi, Kebbi State, Nigeria

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Abstract

The feasibility of using extract of Grewa Venusta (wild jute tree) root as corrosion inhibitor with mild steel was investigated using gravimetric and electrochemical techniques in 1.0 M hydrochloric acid. The inhibitor's concentration, temperature and time were varied in the range of 0-10% v/v at 2% v/v interval, 30 - 75 °C at 15 °C interval and 1-6 hours at 1 hour interval. Characterizations of the extract were done by quantitative method (AAS) and Gas Chromatography-Mass Spectrometry (GC-MS). Scanning electron microscope (SEM) was used to analyze the surface morphology of the samples. The synergetic effect of the inhibitor was evaluated by addition of halide ions (KBr⁻, KCl⁻ and KI⁻). The results showed that corrosion rate increased with an increase in temperature, and decreased with an increase in inhibitor's concentration and time; maximum inhibition efficiency was 97.60% and 99.88% in the presence of KIaddition, and was assumed to occur via adsorption of the inhibitor molecules on the metal surface. The extract contains metallic elements such as calcium, magnesium, mono acetate ($C_5H_{10}O_4$) and 4H-Pyrazole ($C_9H_{10}F_6N_2S$) that suppressed the anodic dissolution. The adsorption of the extract molecules on the mild steel surface obeys Langmuir adsorption isotherm. The results showed that the inhibitor acted as a mixedtype inhibitor.

Keywords: Adsorption isotherm; characterizations; GC-MS; SEM; halide ions.

Introduction

Engineering metals are unstable in natural and industrial environments. In the long term, they inevitably revert to stable chemical species akin to the chemically combined forms from which they were extracted. In that sense, metals are only

^{*} Corresponding author. E-mail address: onoruoizadanjumas@yahoo.co.uk

borrowed from nature for a limited time. Nevertheless, if we understand their interactions with the environments to which they are subjected, and take appropriate precautions, degradation can be arrested or suppressed long enough for them to serve the purposes required by [1]. Iron and steel are the most versatile, least expensive and most widely applied of the engineering metals, and they are unequaled in the range of mechanical and physical properties with which they can be endowed by alloying and heat-treatment [2]. The main disadvantage of iron and most alloys based on it is that they have poor resistance to corrosion in even relatively mild service environments, and usually need the protection of coatings or environment conditioning, according to [3]. This generalization excludes stainless iron and steel that are formulated with high chromium contents to change their surface chemistry.

Metals in service often give a superficial impression of permanence, but all, except gold, are chemically unstable in air and air-saturated water at ambient temperature, and most are also unstable in air-free water. Hence, almost all environments in which metals serve are potentially hostile, and their successful use in engineering and commercial applications depends on protective mechanisms [4]. In some metal/environment systems, the metal is protected by passivity, a naturally formed surface condition inhibiting reaction. In other systems, the metal surface remains active, and some form of protection must be provided by design. The study of mild steel corrosion which researches the most prolific, flexible, versatile and least expensive metallic materials is a matter of tremendous theoretical and practical concern and, as such, has received a considerable amount of interest [5]. Acids are widely used in industrial acid cleaning, descaling and pickling, and oil well acidizing, according to [6], and require the use of corrosion inhibitors, in order to restrain their corrosion attack on metallic materials. However, the applications of mild steel are greatly hindered by pitting and stress corrosion cracking, especially in hostile environments, such as acidic (HCl and H₂SO₄) and halide – seawater. Acid is a good electrolyte and the pH lower than 7 can cause pitting and stress corrosion cracking, as observed by [7].

Several attempts have been made to solve the corrosion problems associated with mild steel in acidic environments, and one of the chosen methods was the use of corrosion inhibitors. However, most of these synthetic compounds show good anticorrosive action, and most of them are highly toxic to both human beings and the environment, according to [8]. The issue of toxicity has led investigations to focus on the use of naturally occurring substances, in order to find low-cost and non-hazardous inhibitors. Plant extracts have become important as an environmentally acceptable, readily available and renewable source of materials for a wide range of corrosion prevention formulations. Therefore, finding naturally occurring substances as corrosion inhibitors is a subject of great practical significance, according to [9-10]. Extracts of plant materials contain a wide variety of organic compounds. Most of them contain hetero-atoms, such as P, N, S, O. These atoms coordinate with the corroding metal atom (their ions), through their electrons. Therefore, protective films are formed on the metal surface and, hence, corrosion is prevented, according to [11]. The inhibition

efficiency of plant extracts, in controlling corrosion of metals in various environments, has been investigated in acidic media [12-16].

In the present work, *Grewa Venusta* extract was found out to be a cheap, ecofriendly and naturally occurring substance, and its inhibitive action on the corrosion behaviour of mild steel in 1.0 M HCl was investigated through Gravimetric - weight loss and Potentiodynamic polarization (Tafel analysis) measurements at 30, 45, 60 and 75 °C in an acidic environment. Kinetic and activation parameters that govern the metal corrosion were evaluated; the coupon surfaces were examined in the absence and presence of the corrosion inhibitor, using Scanning Electron Microscope (SEM), to find out the constituents that were responsible for the inhibition. The plant extract was characterized by Atomic Absorption Spectroscopy (AAS), Quantitative phytochemical screening and Gas Chromatography–Mass Spectrometry (GC–MS).

Experimental procedures

Preparation of the plant extract

The plant *Grewa Venusta* was obtained from Ahmadu Bello University, Zaria, dried, ground and soaked in a solution of ethanol for three days. The filtrate was subjected to evaporation in order to obtain the sample free of ethanol, using an evaporator. The stock solution, 2-10% v/v of the extract, was used to prepare different concentrations of the test solutions dissolved in 1.5 Litres of 1.0 M hydrochloric acid.

Preparation of mild steel specimen

Mild steel rods were mechanically cut into a cylindrical shape of 20 mm by 10 mm, with the chemical compositions shown in Table 1. The specimens were mechanically polished with emery papers of 80 to 800 grades, and subsequently degreased and stored in the desiccators to avoid re-oxidation. Weight of the samples was taken before and after the test.

С	Mn	Si	Р	S	Al	Ni	Fe
0.17	0.45	0.18	0.012	0.032	0.005	0.008	Balance

Table 1. Chemical composition of the mild steel.

Weight loss measurements

Previously polished and degreased specimens of size 20 mm by 10 mm were used for weight loss studies. Already weighed specimens were separately immersed in 250 milliliters (mL) of 1.0 M HCl solutions containing 0, 2, 4, 6, 8 and 10 % v/v of GV extract, for 1, 2, 3, 4, 5 and 6 days. After the elapsed time the specimens were taken out, washed, dried and reweighed. All the experiments were performed in triplicate, and average values were recorded. The experiment was carried out at four different temperatures of 30, 45, 60 and 75 °C, respectively. From the measured weight loss data, the corrosion rate (mm/y) and the inhibition efficiency (IE) were calculated using equations 1 and 2 as in [12]:

$$CR = \frac{KW}{AtD} \tag{1}$$

where $K = 8.76 \times 10^4$ (constant), W = weight loss in g, A = area in cm², t = time in hours, and D = density in g/cm³ (7.86), respectively.

$$IE \% = \frac{c_{R_a} - c_{R_p}}{c_{R_a}} x \, 100 \tag{2}$$

where, CR_a and CR_p are the corrosion rates in the absence and presence of inhibitor.

Electrochemical measurements

The electrochemical measurements were performed in a conventional threeelectrode assembly containing a cylindrical carbon steel specimen with an exposed area of 1 cm² as working electrode (WE); a platinum foil of surface area 2 cm² as counter electrode; and a saturated calomel electrode (SCE) provided with a Luggin capillary as a reference electrode. They were immersed in a 1 M HCl solution until a steady-state open circuit potential (OCP) was obtained. Potentiodynamic polarization measurements were done using an Autolab potentiostat (PGSTAT30 computer controlled) with the General Purpose Electrochemical Software (GPES) package version 4.9. The HCl solution was degassed with ultrapure nitrogen bubbling to avoid any reactions with dissolved oxygen. Tafel polarization measurements were made for a potential range of -200 mV to +200 mV with respect to OCP, at a scan rate of 1 mV/s. From the electrochemical studies, corrosion potential and corrosion current were calculated. All the tests were performed at a temperature of 30 °C. The inhibitor efficiency was evaluated using equation 3 as in [18].

$$IE \% = \frac{i_{corr} - i_{corr}}{i_{corr}} x \ 100\%$$
 (3)

where i_{corr} and i_{corr} are the corrosion current densities of mild steel in the absence and presence of the inhibitor, respectively.

Determination of metallic cations in the extracts using AAS

The Atomic Absorption Spectrophotometer (AAS) was used for the analysis of the following metals: Mg, Zn, Fe, Mn, Cu, Pb and P. Using AAS, a known amount of the sample was placed in a dish and heated with a Bunsen burner in a fume cupboard, until there was no more smoke emitted. This was transferred to the desiccator for it to cool down, after which a 0.1 M HCl solution was added to the ash. The resulting solution was filtered and diluted. Suitable salts of the metals in question were used to make their standards, lamps were fixed and the analyses were done. Using the flame photometer, the sample diluents were aspirated into the jenway digital flame photometer using the filter corresponding to each mineral element. All these were carried out using the method described in [17]. The experiment was carried out at the Industrial Chemical Laboratory, National Research Institute for Chemical Technology, Zaria.

Gas Chromatograph- Mass Spectrometry (GC-MS) analyses

About 1 mL of each extract concentration was analyzed by GC-MS using QP 2010 Plus Schmadzu Product equipped with two fused-silica capillary columns, with 60 m \times 0.22 mm, film thickness, at National Research Institute for Chemical Technology, Zaria. The conditions under which the experiment was carried out were the same as in previous work [12].

SEM investigations

The mild steel surface was prepared for SEM studies by keeping the specimens for one hour in the electrolyte, with and without the optimum concentrations of the inhibitor. The mild steel specimens were then washed with distilled water, dried and analyzed using SEM. A Philips model XL30SFEG scanning electron microscope was used for surface analysis, as described by [15].

Results and discussion

Determination of phytoconstituents of the GV

The results obtained from the quantitative method are presented in Table 2:

Table 2. Analytical results of phytochemical screening of the Grewa Venusta (GV).

S/N	Plants	Alkaloids	Tannins	Saponins	Flavonoids	Glycosides	Volatile oil
1	G.V	1.21±0.45	14.65±0.52	2.99±0.87	0.96±0.59	0.43±10	0.77±0.21

Determination of metallic elements in the extracts using AAS

Table 3 gives the metallic elements present in the *Grewa Venusta* extract, determined using Atomic Absorption Spectrophotometer (AAS).

Table 3. Chemical compositions of *Grewa Venusta* extract (metallic cations) from AAS analysis.



Figure 1. Chromatogram and corresponding mass spectra of *GV* extract showing the peaks of the compounds.

Gas Chromatography- Mass Spectrometry (GC-MS) analyses

Tables 4 and 5 show the results of GC–MS data of extract compounds identified in the ethanol distillate of GV by GC-MS analysis, while Figs. 1 and 2 show the GC-MS spectra and the structures of the compounds identified in the extract.

				Peak 1	Report HC			
Peak	R time	I time	F. time	Area	Area %	Height	Height %	A/H
1.	5.119	5.083	5.217	134883	2.57	53829	6.23	2.51
2.	8.068	8.017	8.208	1201168	22.84	262173	30.34	4.58
3.	9.952	9.892	10.225	536040	10.19	54313	6.29	9.87
4.	13.182	13.067	13.458	681543	12.96	48799	5.65	13.97
5.	15.736	15.60	16.067	1585941	30.16	156761	18.14	10.12
6.	19.039	18.983	19.125	165650	3.15	54801	6.34	3.02
7.	20.250	20.167	20375	538550	10.24	130800	15.14	4.12
8.	22.526	22.475	22.592	101864	1.94	37913	4.39	2.69
9.	23.142	23.058	23.200	312818	5.95	64587	7.48	4.84
				5258457	100.00	863976	100.00	

Table 4. GC–MS data of Grewa Venusta ethanolic extract.

Table 5. Chemical compounds identified in the ethanol distillate of *Grewa Venusta* (GV)) extract by GC-MS analysis.

Peaks	Extract	Compounds name	Molecular formula	Molecular weight g/mol
1		2-Pentanone, 4-methoxy-4-methyl	$C_7H_{14}O_2$	130
2		4H-Pyran-4-one, 2,3-dihydro-3	$C_6H_8O_4$	144
3		1,2,3-Propanetriol, mono acetate	$C_5H_{10}O_4$	134
4		4H-Pyrazole, 3-tert-butylsulfanyl-4	$C_9H_{10}F_6N_2S$	292
5	Grava	Dodecanoic acid, 3-hydroxy-	$C_{12}H_{24}O_3$	216
6	Venusta	Hexadecanoic acid, 15-methyl-	$C_{18}H_{36}O_2$	284
7	(GV)	Octadecanoic acid, Stearic acid	$C_{18}H_{36}O_2$	284
8		Cyclohexanol, 3,5-dimethyl	$C_8H_{16}O$	128
9		1,9-Nonanediol, dimethanesulfonate	$C_{11}H_{24}O_6S_2$	316

Weight loss studies

Corrosion parameters obtained from weight loss method are presented in Table 6. The results indicate that the corrosion rates of mild steel decrease with an increase in the concentration of ethanol extract of *Grewa Venusta*. Also, the inhibition efficiency of *Grewa Venusta* decreases with an increase in temperature [11, 18]. Fig. 3 shows the variation of inhibition efficiency with the extract in the presence of the corroding medium. The optimum concentration for *Grewa Venusta* was found to be 8% v/v with maximum inhibition efficiency of 97.90% for the period of 3 hours of immersion time. This result indicated that the plant extract could act as effective corrosion inhibitor for mild steel in 1.0 M HCl, due to the compounds/elements determined by both analytical /quantitative method, AAS and GC-MS, shown in Tables 1, 2 and 4, respectively, supported by Figs. 1

and 2 [7,8,11,12]. The effect of immersion time was studied for periods of 1h to 6h, as shown in Table 7; it reveals that the plant extract showed maximum efficiency at 3h of immersion time (as also illustrated in Fig. 4,) which is sufficient for the pickling process [16]. However, this behaviour has been attributed to the increase in the elements/compounds that form stable oxides. The thin layer of the oxides adhered to the metal surface, resulting in a decrease in the corrosion rate. Similar results have been reported by [14, 16].



Peak 9: 1,9-Nonancdiol

Figure 2. Structures of the compounds (peaks 2, 1, 4, 5, 7, 9) present in GV.

Table 6. Corrosion rate, inhibition efficiency (% IE) and surface coverage for mild steel in a 1.0 M HCl solution, with and without a varying concentration of *Grewa Venusta* extract at 30 $^{\circ}$ C for 6 days.

Conc (% v/v)	Corrosion rate (mmpy)	Inhibition eff.; %IE	Surface cov. (0)
Blank	51.712	-	-
2	9.943	80.77	0.81
4	7.751	85.01	0.85
6	4.767	90.78	0.91
8	1.085	97.9	0.98
10	1.768	96.58	0.97

Table 7. Effect of immersion time on inhibition efficiency of mild steel in 0.5 M H ₂ SC)4
at 30 °C in the presence of optimum concentrations of the GV extract.	

Optimum	Inhibition efficiency (IE %)					
concentrations	Immersion time (h)					
	1 h	2 h	3 h	4 h	5 h	6 h
8% v/v of Grewa Venusta	85.89	92.71	97.9 0	97.75	96.54	95.98



Figure 3. Variation of inhibition efficiency against concentration of extracts at $30 \ ^{\circ}C$.



Figure 4. Variation of inhibition efficiency of GV extract in 1.0 M HCL `with immersion time.

Potentiodynamic polarization measurements

The typical Tafel polarization curves of mild steel in 1.0 M HCl, in the presence and absence of *Grewa venusta* (wild jute tree) at different concentrations, are shown in Fig. 5.



Figure 5. Potentiodynamic polarization curves for mild steel in 1.0 M HCl solution in the absence and presence of various concentrations of the GV extract at 30 °C.

The polarization study showed that there was the formation of a protective film formed on the metal surface during corrosion inhibition process, as observed by [12, 17]. It could also be observed that both the cathodic and anodic reactions were suppressed with the addition of *Grewa Venusta*; this resulted in a protective

film formed on the metal surface, thereby decreasing the corrosion current value (Icorr). This also suggests that *Grewa Venusta* reduced anodic dissolution, and also effectively retarded the hydrogen evolution reaction. The corrosion parameters, including corrosion current densities (Icorr), corrosion potential (Ecorr), cathodic Tafel slope (bc), anodic Tafel slop (ba) and inhibition efficiency (EI %), were calculated using equation 3 [18].

Weight of	Ecorr	Icorr	Tafel	mV/decade	Inhibition
extract (gm)	/ mV	/(mA/cm ²)	slopes	bc	efficiency
Blank (0)	-0.531	4.242	0.169	0.066	-
2.00	-0.577	0.9706	0.147	0.128	75.12
4.00	-0.565	0.7025	0.118	0.144	83.44
6.00	-0.549	0.4832	0.126	0.162	88.61
8.00	-0.552	0.3203	0.137	0.147	92.45
10.00	-0.573	0.2825	0.148	0.154	93.34

 Table 8. Potentiodynamic polarization parameters for mild steel in 1.0 M HCl containing different concentrations of GV extract, at 30 °C.

The visual examination of polarization curves depicted in Fig. 5 reveals that the corrosion current density decreased as the inhibitor's concentration increased. However, the corrosion potential shifted more markedly to a negative direction. Generally, if the displacement in Ecorr is higher than 85 mV with respect to Ecorr in an uninhibited solution, the inhibitor can be seen as of a cathodic or anodic type, as observed by [19, 20]. From Table 8, the maximum displacement was 46 mV, which indicates that GV acts as a mixed-type inhibitor at 30 °C. It also shows that the effect of the inhibitor on the cathodic reaction is more observable than on the anodic reaction, and that the inhibition efficiency increased from 75.12% to 93.34% with the increment of GV concentration. Thus, this inhibitor acts as a mixed type inhibitor, and this agrees with the works of [19, 21].

Adsorption isotherm

It is evident that the corrosion inhibition process is based on the adsorption of the inhibitor molecules on the metallic surface. Generally, two modes of adsorption were always considered. Physical adsorption requires the presence of electrically charged metal surface and charged species in the bulk of the solution, while chemisorption requires charge sharing or charge transfer from the inhibitor molecule to the metal surface. In order to specify the adsorption mode of *Grewa Venusta* molecules on the mild steel surface in the acidic solution, the degree of surface coverage (θ), at different concentrations of the inhibitor (% v/v) in the stagnant aerated acidic solution, was determined from the corresponding weight loss measurements, according to eq. 2 [12, 19]:

The obtained values of θ were fitted to different isotherms, including Langmuir, Frumkin, El-Awady and Temkin isotherms. The best fitting was found to obey the Langmuir adsorption isotherm in equation 4, which is based on the assumption that all adsorption sites are equivalent and that particle binding

occurs independently from nearby sites being occupied or not, as noted by [17, 20]:

$$\frac{\theta}{1-\theta} = K_{ads}C \tag{4}$$

where C is the concentration of inhibitor, θ the fractional surface coverage and K is the adsorption equilibrium constant related to the free energy of adsorption ΔG_{ads} , as shown in previous work of [22]:

$$\Delta G_{ads} = -2.303 RT \log (55.5 K)$$
(5)

where R is the molar gas constant, T the absolute temperature, the value 55.5 is the concentration of water in a solution, expressed in mol.L⁻¹, and K is the equilibrium constant. A plot of C/ θ as a function of C gives a straight line with a slope of almost unity. Such linear relationship was verified for the adsorption of *Grewa Venusta* on the mild steel surface, as shown in Fig. 6.

Table 9. Parameters from Langmuir isotherm for *GV* at 30, 45, 60 and 75 °C in 1.0 M HCl solution.



Figure 6. Langmuir adsorption isotherm for the adsorption of the *GV* inhibitor on the mild steel surface in 1.0 M HCl solution by gravimetric method at 30, 45, 60 and 75 °C.

The free energy of adsorption, ΔG_{ads} , equilibrium constant, K_{ads} , coefficient of correlation, R^2 and slopes were presented in Table 9. It is also evident that the values of equilibrium constant are relatively small and decrease with an increase in temperature, as seen from Table 8, suggesting that the interaction between the adsorbed extract molecules and mild steel surface was physisorption, which also agrees with findings of [2, 22]. Other researchers, such as Suleiman et al. [12], claimed that any values around -20 kJmol⁻¹ or less negative are consistent with electrostatic interaction (physisorption), while those around -40 kJmol⁻¹ or more negative involve chemisorption, which was also supported by Khamis et al. [25].

Therefore, the adsorption of the investigated *Grewa Venusta* inhibitor molecules on mild steel is of a physical nature.

Kinetics/thermodynamics consideration

In order to study the effect of temperature on the inhibition adsorption mechanism of *Grewa Venusta* in an acidic solution, in absence and presence of 2-10% v/v, studies were carried out at different temperatures (303-348 K), by weight loss measurements during 6 days of immersion time. It was noticed that the corrosion rate increases both in the uninhibited and inhibited solution, with an increase in temperature. The presence of inhibitor leads to a decrease in the corrosion rate, and inhibition efficiency also decreases with an increase in temperature, meaning that the corrosion process is temperature dependant, as observed by [24].

The results obtained are presented in Table 10 and illustrated in Fig. 7.

Table 10. Effect of temperature on mild steel corrosion in the presence and absence of 8% v/v of *Grewa Venusta* extract for 6 days.

	Corr. rate in the absence of GV (CR ^o)	Corr. rate in the absence of GV (CR)	Inhibition efficiency (%IE)
Temp.(
K)			
303	51.712	1.085	97.90
318	54.316	5.611	89.67
333	57.319	7.577	86.78
348	59.873	13.441	77.55

It can be seen that the inhibition efficiency decreased with an increase in temperature. This might be due to the increased rate of the dissolution process of mild steel and partial desorption of the inhibitor from the metal surface with temperature. This occurrence has been reported elsewhere [18, 24].



Figure 7. Variation of inhibition efficiency of extracts with temperature in a 1.0 M HCl solution.

In the presence of the extract, the inhibition efficiency increased up to a temperature of 303 K, and after that there was a decline from 318 - 348 K. Maximum inhibition efficiency was found to be 97.70% and minimum of

77.55%, with 8% v/v concentration of *Grewa Venusta* extract in an acidic solution with mild steel. From previous studies [25, 26, 27], adsorption and desorption of inhibitor molecules continuously occur at the metal surface, and an equilibrium exists between these two processes at a particular temperature. This shows that there is an active-passive region in the corrosion process of mild steel in the studied environment.

It has been observed that as adsorption decreases, more desorption of the inhibitor occurs, because these two opposite processes are in equilibrium [24]. Due to a greater desorption of inhibitor molecules at higher temperatures, the bigger surface area of the mild steel in contact with aggressive environment (HCl) results in an increase in corrosion rates, with an increase in temperature; similar works have been reported [22, 28].

Accordingly, the effect of temperature change in such condition of inhibited acid-metal reaction is not uncommon. Equally, the inhibitor itself may undergo decomposition reaction. In an acidic solution, the corrosion rate is related to temperature by Arrhenius equation given in equation (6) [12]:

Log(CR) = -Ea/2.303RT + A (6)

where Ea is the apparent effective activation energy, R is the general gas constant and A is Arrhenius pre-exponential factor. A log plot of the corrosion rate obtained by weight loss measurement versus 1/T gave a straight line with a slope of (-Ea/2.303R) presented in Fig. 8. The values of activation energy are presented in Table 11, and the data show that the activation energy (Ea) of the corrosion rate of mild steel in 1.0 M HCl solution in the presence of the extract is higher than that in an uninhibited solution. The increase in the apparent activation energy for mild steel dissolution in an inhibited solution in this study may be interpreted as physical adsorption, which supports our earlier claim. It was also reported that an increase in the activation energy is attributed to an appreciable decrease in the adsorption of the inhibitor on the metal surface with an increase in temperature [24]. An alternative formulation of Arrhenius equation, given in equation (7) [12], was used to calculate Δ Hads and Δ Sads:



Figure 8. Variation of log CR with 1/T for mild steel in 1.0 M HCl in the presence and absence of *GV* concentration at 30, 45, 60 and 75 °C.

Fig. 9 shows the log plots-(CR/T) versus 1/T, which is a straight line with the slope and intercept equal to $-\Delta$ Hads/2.303R and (log(R/Nh) + Δ Sads/2.303R), respectively.



Figure 9. Variation of log CR/T with 1/T for mild steel in 1.0 M HCl in the presence and absence of *GV* concentration at 30, 45, 60 and 75 °C.

Table 11. Activation parameters Ea, $\Delta Hads$ and $\Delta Sads$ for mild steel dissolution i	n 1.0
M HCl in the absence and the presence of GV at 30, 45, 60 and 75 °C.	

System/concentration	Ea (kJmol ⁻¹)	∆ <i>Hads</i> KJ/mol	∆Sads (J/mol.K)
Blank	2.872	4.442	-172.972
2% v/v GV	15.796	7.487	-167.457
4% v/v GV	15.781	7.276	-168.893
6% v/v GV	25.849	9.899	-161.388
8% v/v GV	38.084	12.292	-154.744
10% v/v GV	46.528	13.786	-132.383

From Table 11, it can be seen that values of $\Delta Hads$ and $\Delta Sads$ are positive and negative. The positive sign of $\Delta Hads$ indicates that the adsorption of the inhibitor molecules is an endothermic process. The values of $\Delta Sads$ in the presence of *Grewa Venusta* are negative, meaning that a decrease in disordering takes place on going from reactants to the metal adsorbed species reaction complex, as observed in [11]. Still on Table 11, the values of Ea determined in the presence of *Grewa Venusta* are higher (46.528 kJ mol⁻¹) than those of the uninhibited solution (2.872 kJ mol⁻¹). The increase in the activation energy may be interpreted as physical adsorption, which satisfied our earlier claimed supported by previous works [11, 28].

Surface morphology and adsorption isotherm

The morphology of the samples without and with inhibitor of *Grewa Venusta* were examined and presented in Figs. 10a and 10b. From the surface morphology of uninhibited mild steel in 1.0 M HCl interface in Fig. 10a, severe pits, cracks and selective dissolution of intermetallic occurred, whereas there was an improvement in the surface morphology of mild steel treated with the inhibitor, in Fig. 10b. From the SEM evaluation, it is clear that some of the active constituents ($C_7H_{14}O_2$, $C_9H_{10}F_6N_2S$, $C_{18}H_{36}O_2$, $C_{11}H_{24}O_6S_2$, many O-heterocyclic rings) act as reaction centers, leading to the formation of a film on the surface of the mild steel, as proved by [25]. The inhibitor, therefore, forms protective thin layers and complexes on the mild steel surface.



Fig.10. SEM microstructure of mild steel immersed in (a) 1.0 M HCl; (b) in1.0 M HCl with 8% v/v of *Grewa Venusta*.

Synergism parameter

The increase in the inhibition efficiency of organic compounds in the presence of some anions has been observed and was ascribed to synergistic effect. On that note, we considered it necessary to incorporate some halides (KBr⁻, KCl⁻ and KI⁻) into the environment. It was observed that KI⁻ performed better than KBr⁻ and KCl,⁻ as shown in Table 12 and illustrated in Fig. 11, respectively. The inhibition efficiency of the system increased in the presence of halide ion (KI⁻) at the studied temperatures interval.

Table 12. Influence of halide additive (0.5 M) on the inhibition efficiency of optimum concentration (8% v/v) of *GV* at different temperatures.

Temp (°C)	GV	GV + KI
30	97.9	99.88
45	89.67	95.89
60	86.78	90.75
75	77.55	81.97



Figure 11. Influence of halide additive (0.5 M) on the inhibition efficiency of optimum concentration (8% v/v) of *GV* at different temperatures.

It was observed that halide ions are normally adsorbed on the surface of a corroding metal, which promotes the adsorption of organic compounds by forming intermediate bridges between the positively charged metal surface and the positive end of the organic molecule. Thus, the inhibitor is adsorbed on the metal by coulombic attraction to the adsorbed halide ions on the metal surface [12, 24].

Conclusions

The following conclusions can be drawn from the study:

- 1. The characterization of the plant extract by GC-MS shows that the spectra revealed the presence of phenolic compounds like tannins, alkaloids and the aromatic compounds 2-pentanone (22.84 %), 1,2,3-propanetriol1, 4H-pyrazole, dodecanoic acid, stearic acid, and 1,9-nonanediol. The Atomic Absorption Spectroscopy (AAS) revealed the presence of calcium (greater than 77%), followed by magnesium (16%), manganese and chromium, while others appear to be minor.
- 2. Reasonable inhibition efficiencies were exhibited by the plant extract, with the corrosion rate decreasing with an increase in the concentrations of inhibitor.
- 3. The Langmuir adsorption isotherm fits the experimental data obtained in this study. Hence, a monolayer film was formed on the mild steel surface by the extract.
- 4. Based on Ea, Δ Gads, Δ Hads and Δ Sads values obtained in this work, physical adsorption phenomena can be proposed for the adsorption of the inhibitors.
- 5. Among the halides ions used, iodide has the best influence on the *Grewa Venusta* extract with highest inhibition efficiency of 99.88%.
- 6. The results obtained using different corrosion analyses (gravimetric and potentiodynamic polarization) are in good agreement.

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